Low Charge NH₃ Evaporators

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Definition: Any NH_3 system which requires a specific system charge of less than (1.3kg / kW)

- Conventional LR system ~ 2.0 3.5kg / kW
- Presently Low Charge systems are between 65g 1.0 kg / kW
- Possible reductions of up to 50 times the currently installed scenario
- Achievable with either reduced recirculation rates or DX feed
- Definition should be reconsidered as 1.3kg / kW, is now actually fairly high
- Opportunities exist not only for Industrial Refrigeration, but also for HVAC and Commercial Refrigeration



What is a "Low Charge Evaporator?"

- There is no such thing!
- Essentially we are only talking about the mass flow through the evaporator
- For low recirculation rates this is less than "historical values"
- As a manufacturer this is our concern
- Coil circuiting is unlike a traditional LR evaporator
- DX remains "unchanged"
- Feed type, or the rate into the coil will determine residence mass in coil

- Ammonia has unique thermophysical properties, combined with a high latent heat of vaporization (= relatively low mass flows)
- Separation of the liquid and vapor phases can occur at low fluid velocities due to the high ratio of vapor to liquid specific volume
- Coil circuiting (fluid velocities) if not correct will cause liquid to settle on lower portion of tubes and render upper portions "dry" resulting in poor evaporator performance (stratified, slug, wavy flow)





- Annular flow is the coil designer's goal in order to:
 - $\circ~$ Maintain inner tube walls wetted
 - $\circ\,$ Maximize the coil performance...
 - …Fluid velocities / coil circuiting (heat flux) are critical to achieve maximum coil thermal performance



Effects of Mass Specific Vapor Quality in Coil;

- If the recirculation rate (RR) is 1:1 all the refrigerant evaporates, and vapor quality (x) at exit is 1.0 [NOT superheated]
- When the recirculated rate is > 1.0 not all the refrigerant is evaporated, only the portion = 1/RR;

- Therefore: as RR is increased, the vapor quality decreases...
- ...AND internal heat transfer co-efficient decreases

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Effects of Reduced Recirculation Rates;

- As can be seen in previous slides the HTC value increases considerably when going from 4:1 to ~1.2:1
- 1:1 is very unlikely, and almost impossible to maintain
- Fluctuations in load will have an impact on coil performance
- However, 1.2:1 is realistic and fairly easy to achieve
- This "minimum" recirculation rate is dependent on tube diameter / geometry
- Coil circuiting, and liquid feed into coil, is different for these reduced rates, and unique for each coil
- Bottom line though, is that on average 5 10% increase in coil performance can be achieved with a 1.2:1 vs. 3.5:1 recirculation rate

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Direct Expansion considerations;

- Traditionally DX coils have always been superheat controlled
- Thermal expansion valves are "history" and have been replaced with Electronic expansion valves
- Superheat values have never been less than ~ 6K
- The superheated vapor portion of the coil surface area provides negligible refrigeration effect (essentially "wasted" surface area)
 [5 – 15%]
- Advancements to control(s) and metering devices has changed this landscape



Direct Expansion considerations;

- Significantly reduces the refrigerant charge
- No mechanical pumps
- Smaller pipe diameters
- Reduced insulation costs
- No separation vessels, but...
- Suction accumulator is recommended



Residence Mass in Evaporator Coil;



"New" Controls Available for DX Applications?

- Vapor Quality sensor, for
 - DX applications, and
 - Low recirculated rate liquid metering
- Measures vapor quality [Void Fraction] NOT a superheat controller
- Built in microprocessor which sends a 4 20mA signal proportional to sensor's determined measurement area
- Advancements to controls and technologies have changed this landscape



Direct Expansion Considerations;

- Having refrigerant leave coil at vapor quality of 1.0 would be "optimum" >>> zero superheat
- With Superheat control this is not possible
 - Even with Electronic valves
- With Vapor quality control this is possible
- However, with vapor quality control consideration should be allowed for "some" liquid carry over (suction accumulator)



Summary;

- The Industrial Refrigeration Landscape as we once knew it has changed!
- End Users and Owners are Striving for;
 - ✓ Reduced Energy Usage
 - ✓ Lower Initial Investment
 - ✓ Reduced Life Cycle Running Costs
 - ✓ Reduced Regulatory Requirements
 - ✓ Inherently Safer NH₃ Systems Installed



Summary – Low RR vs. DX;

Pros – Low RR

- Less coil surface area
- Water in system minimal effect
- Lower operating costs

Pros – DX

- Reduced refrigerant inventory
- Precise feed control
- Suction accumulator only vessel
- No pumps
- Smaller pipe sizes

Cons – Low RR

- Vessels are still required
- Pumping power
- Larger pipe diameters (vs. DX)
- Feed rate control questionable
- Orifice diameters (hot gas defrost)

Cons – DX

- More coil surface area (cost)
- Coil circuiting on large evaporators
- Liquid carry over
- Water (or oil) in the system unstable operation



Summary;

- Lower Recirculation rates are possible, and more advantageous
- NH₃ DX systems today are now reliable due to the advancements in controls and technology
- NH₃ DX is certainly the preferred direction to take

- Güntner is committed to continued research and development to meet the requirements of this changing landscape
- Güntner is committed to being a front-runner in low charge refrigeration systems



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