

Practical experience with a centralized 3 stage NH₃ DX-plant

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Agenda

- Company profile
- The plant
- General argument topics pump to DX system
- Design considerations

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Profil D+B

D+B

Mittelständiges Familienunternehmen

120 Mitarbeiter

Tradition und Expertise seit über **35** Jahren

Ausbildungs- und Weiterbildungsbetrieb

Investitionen in eigene Innovationen

Vollumfängliche Kundenbetreuung

Einsatz von umweltfreundlichen natürlichen Kältemitteln **NH₃** und **CO₂**

24/7/365 Notdienst

Profil D+B



Nahrungsmittel

- Schlachthöfe
- Verarbeitung



Getränkeindustrie

- Brauereien
- Molkereien



Kühlhäuser - Logistik

- TK-Lager
- NK-Lager
- Verteilung NK/TK



Froster

- Schockfroster
- Palettenfroster
- Plattenfroster
- Spiralfroster



Planung

- Entwurfsplanung
- Ausführungsplanung
- Genehmigungsunterstützung



Sonderanlagen

- Absorber NH₃-H₂O
- ATEX Ausführung
- Getriebeschraube mit Gasmotoren

Profil D+B



Technisches Büro
• Planung
• Kalkulation
• Abwicklung



Leitungs-/Stahlbau
• Einbringung und Montage
• Leitungstrassen
• Gestelle und Geländer



Service- und Wartung
• Inbetriebnahme
• Inspektion, Wartung und Reparatur
• Fernwartung



Elektrotechnik
• Planung
• Programmierung
• Visualisierung

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The plant

The beginning of the project:

- Project started as a tender
- 3 stage centralized ammonia liquid pump design
- Quotation of tender and an alternative with DX

The plant

Basic information:

Evaporation temperature

- -10°C
(+14F)
- -32°C
(-25F)
- -42°C
(-44F)

Room volume

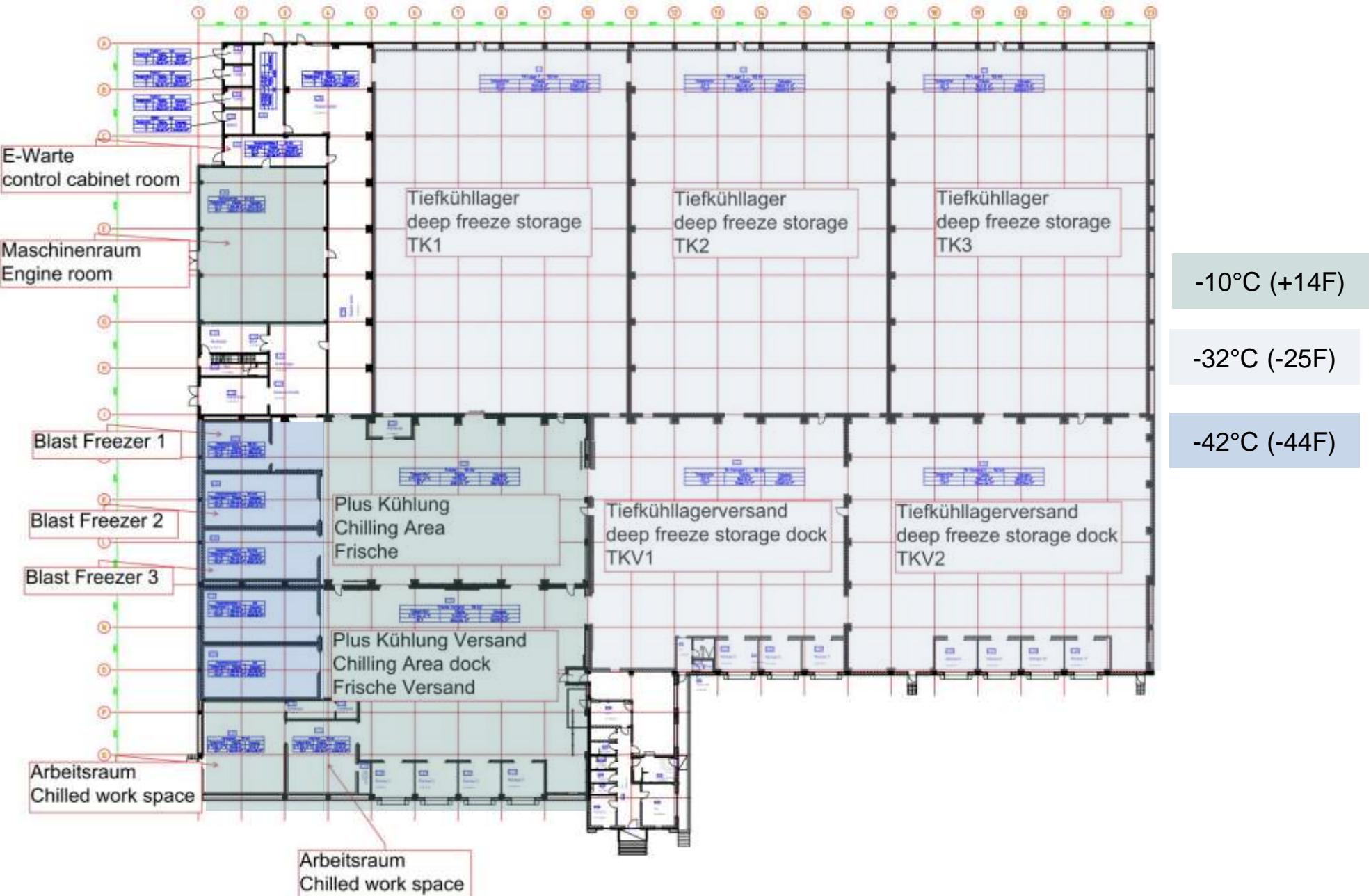
- 10.620m³
(374.800 ft³)
- 80.840m³
(2.855.000 ft³)
- 1.345m³
(386.000 ft³)

Cooling capacity

- 484kW
(136TOR)
- 760kW
(215TOR)
- 615KW
(174TOR)

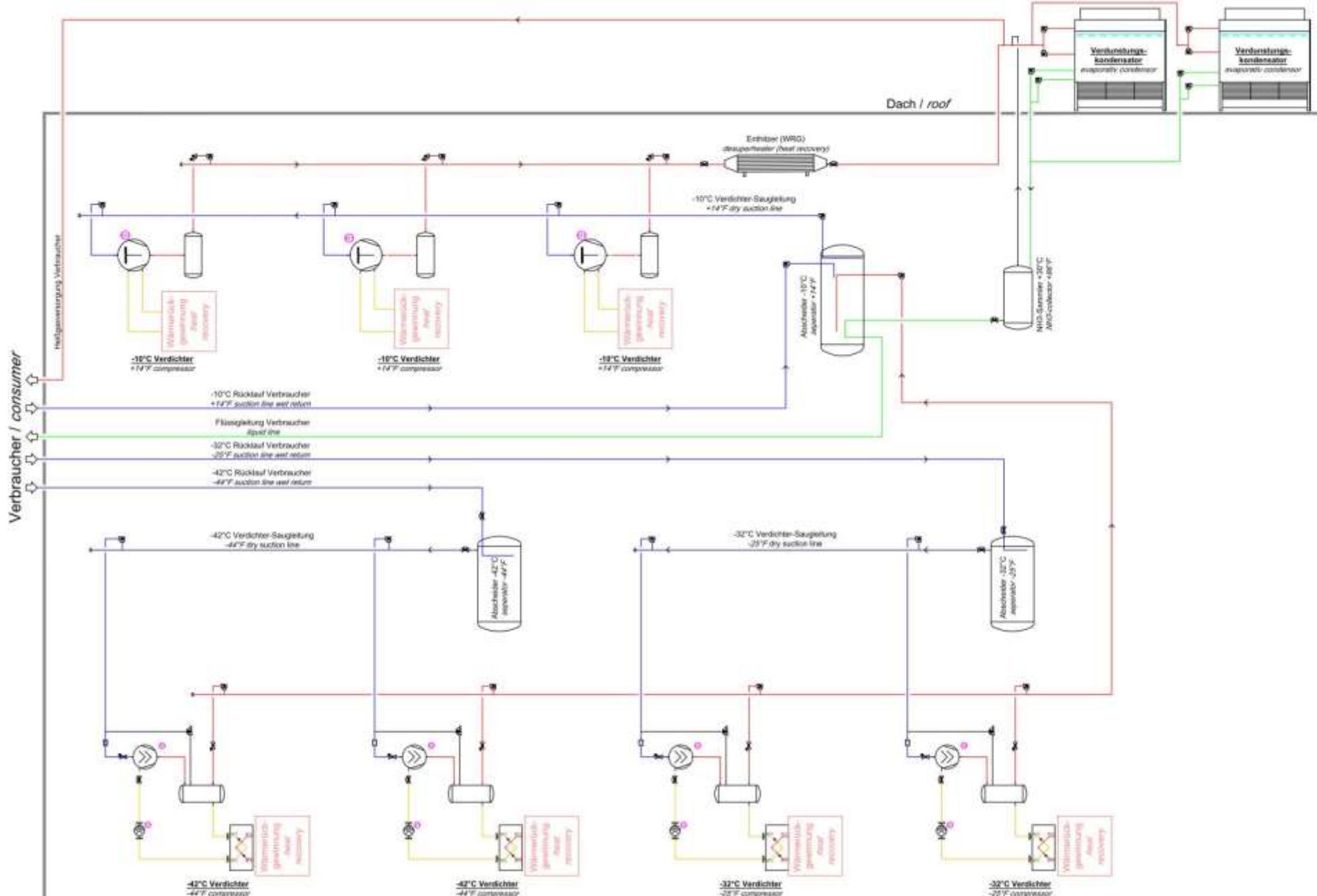
The plant

Layout



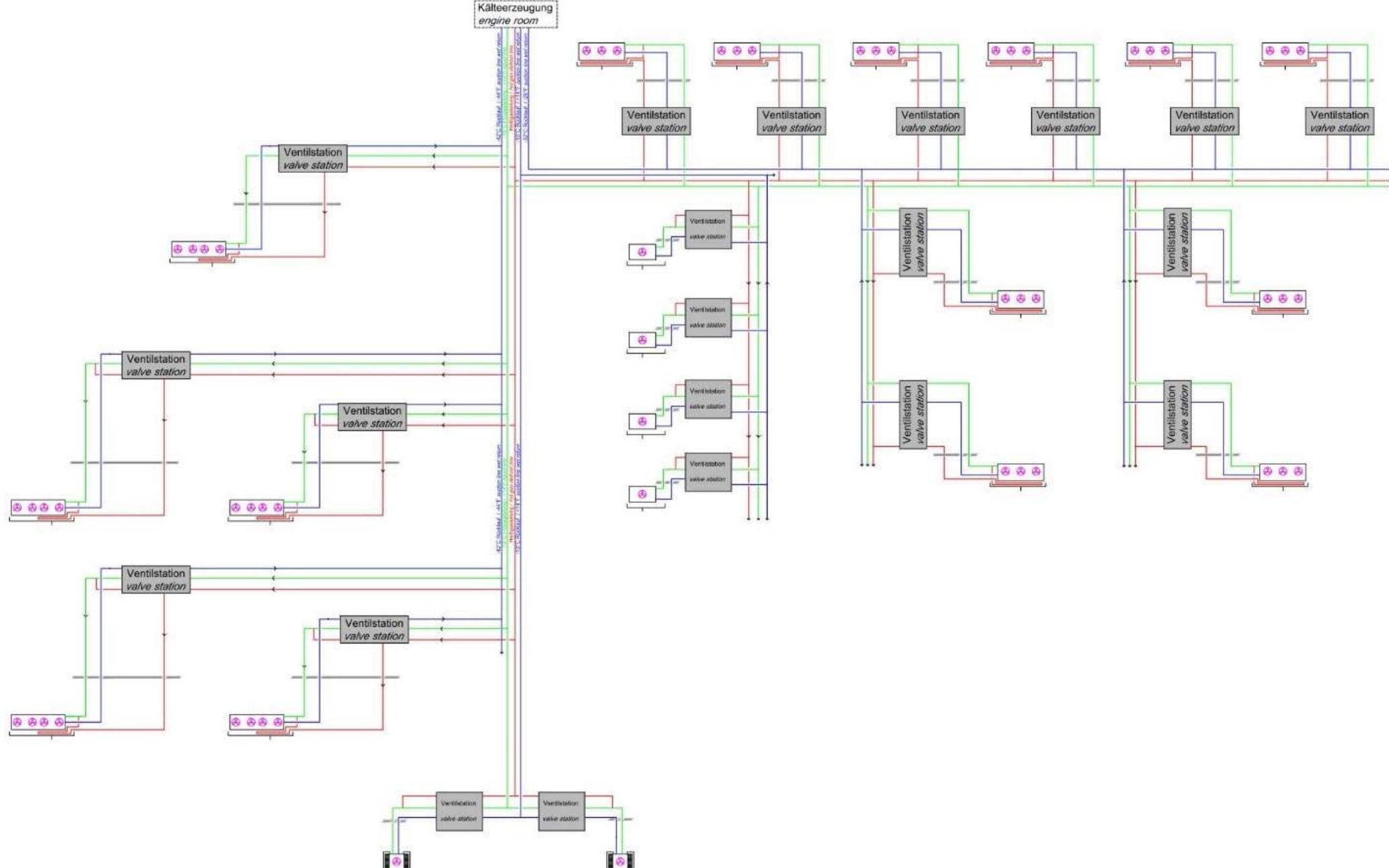
The plant

P&ID



The plant

P&ID



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- **General argument topics pump to DX system**
- Design considerations

General argument topics pump to DX system

Number	Topic	Argument
1	DX more efficient	No ammonia pumps Dry suction riser Smaller pipe dimensions
2	Liquid management	Where to place the liquid Seperator or overheat
3	Defrost	Hotgas -> liquid manag. Elektrik Water or other
4	Cost benefit	Investmentcost higher Operationacost lower

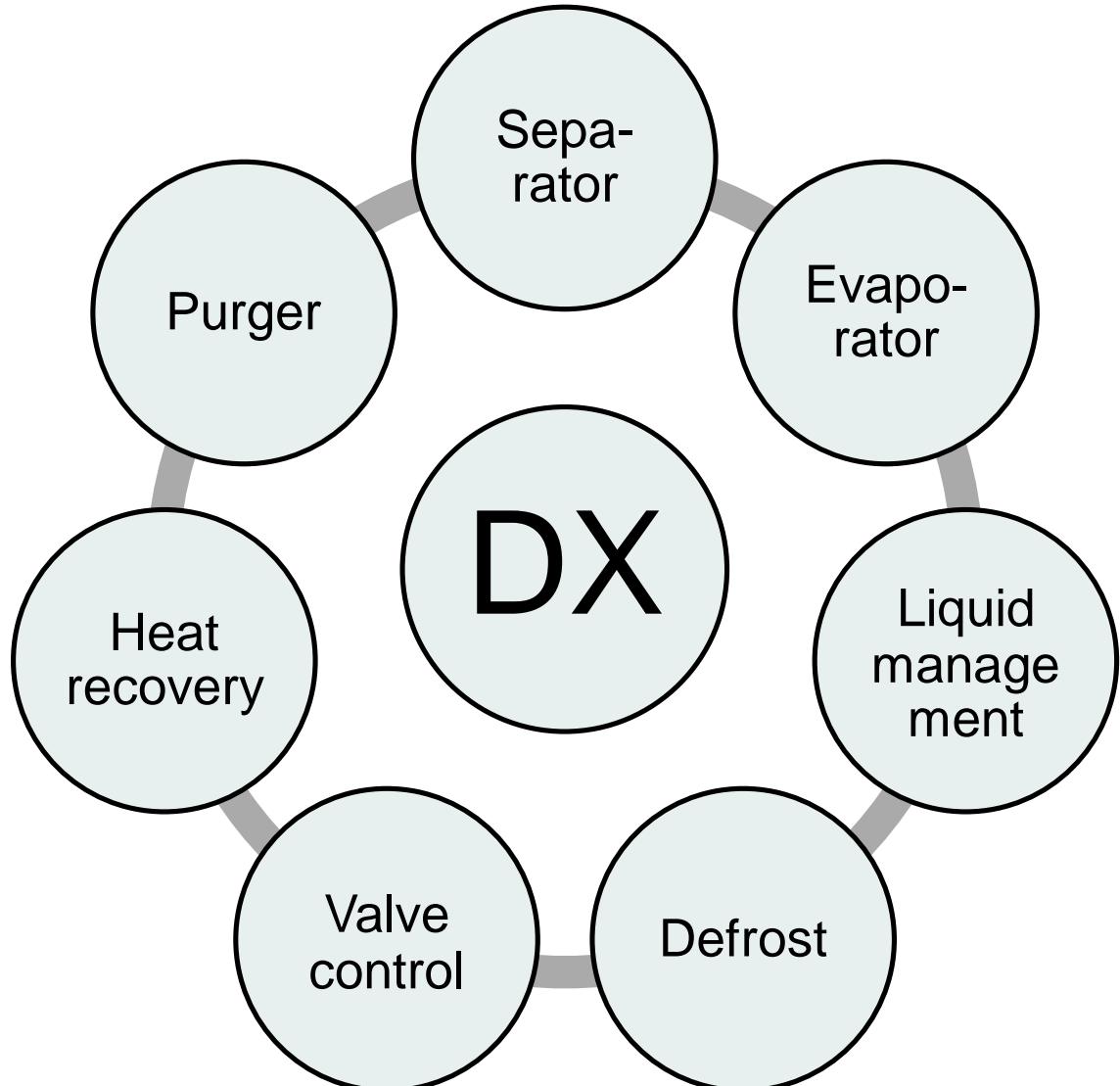
General argument topics pump to DX system

Number	Topic	Argument
5	Operational cost savings	Comparing concepts Comparing plants SEC
6	Energy saving	15%+ possible
7	Measurng energy	Not possible for 2 phase fluids
8	Refrigerant charge	Reduction from 5 to 2,2t

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Design considerations



Design considerations

Evaporator

- Material mix
- Overheat
- Refrigerant in / out position
- Sensor position
- Hotgas defrost
- Refrigerant distributor

Design considerations

Liquid management

- Hotgas condensate
- Condensate due to pressure changes
- Evaporator start up liquid
- Condensate due to still stand in cold surroundings

Design considerations

Valve control

- Overheat control
- Moist control
- Liquid feed control
- Evaporator start up
- Multiple sensor
- Cooling restart after defrost

Q&A

Q

&

A



**eurammon e. V. is always available as a sparring partner for questions
on refrigeration with natural refrigerants.**

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